



Food waste to H_2 Biorefineries as a tool for environmental innovation

Joana R. Ortigueira

1.

Context & Introduction



The problematic of food waste

Food Waste

Raw or cooked food lost before, during or after meal preparation, as well as food discarded in the manufacturing/production, distribution, wholesale/retail and food service sectors



Causes

1. Overproduction & faulty production
2. Inadequate marketing rules and strategies
3. Deficient stock management
4. High appearance standards

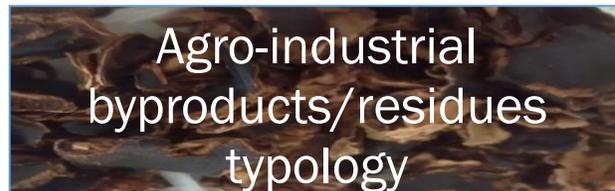


Impacts

- A. Waste of resources
- B. Environmental impact
- C. Cost of treatment and disposal



Directly affects food security
and availability

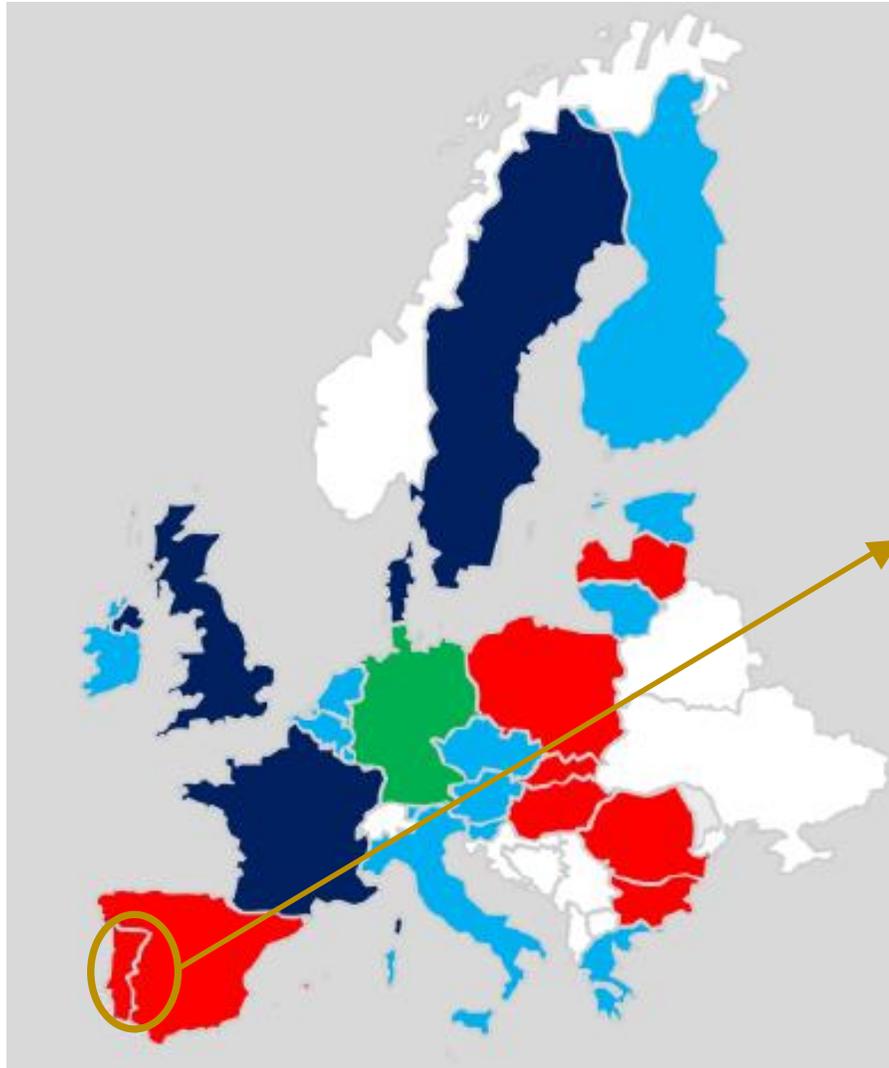


- Less variable chemical characterisation
- Generally with set valorisation/disposal methods
- Highly dependent of cultivated cultures



- Highly dependent of the local diet, culture and territory
- Chemical characteristics dependent of seasonality
- High water content (>70-80%)
- Extremely heterogenous

Food waste quantification and disposal



At the EU-28 level (*per year*):

1.031

**Mt of food waste
produced in the
Portuguese territory**

kg CO₂ eq. per capita

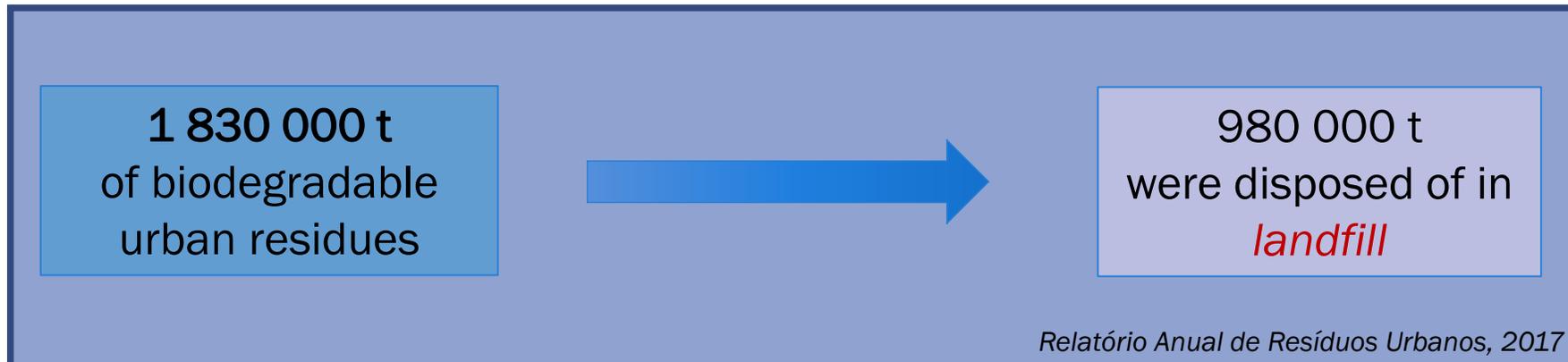
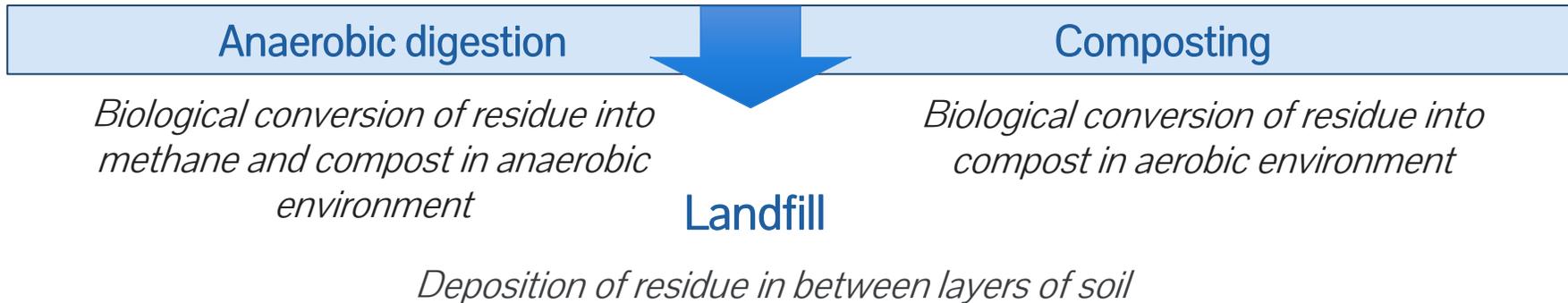
143 billion €

Economic loss

In 2017, 39% of the portuguese urban residues were classified as bioresidues



42% of the biodegradable urban residues valorised



Relatório Anual de Resíduos Urbanos, 2017

Biological process disadvantages

- Production of CO_2 and H_2S
- Release of CH_4
- Extensive process duration (2-10 weeks)

Biogas conversion disadvantages

- Production of NO_x and CO_2
- Release of non-converted fuel (CH_4)
- Low efficiency of fuel combustion (20-30%)

Waste management guidelines

*“Member States shall not accept the following waste in landfills for non-hazardous waste by 1 January 2025, recyclable waste including plastics, metals, glass, paper and cardboard, and other **biodegradable waste**.”*

Amendment to 1999/31/EC on the landfill of waste

ERL codes (European residue list): ERL 010203, ERL 020203, ERL 020304, ERL 020501, ERL 020601

Material degradable
through biological
decomposition



FOOD WASTE

Carbohydrates

Proteins

Fat

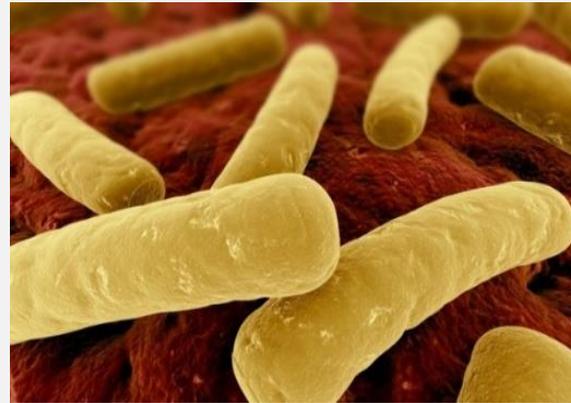
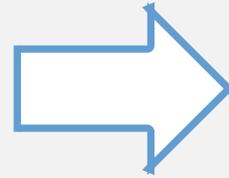
Assorted functionalised
compounds

2.

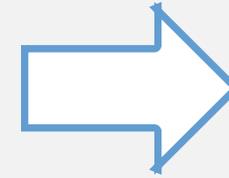
Acidogenic fermentation as valorisation system



Dark fermentation as valorisation system



Anaerobic bacteria



Organic acids

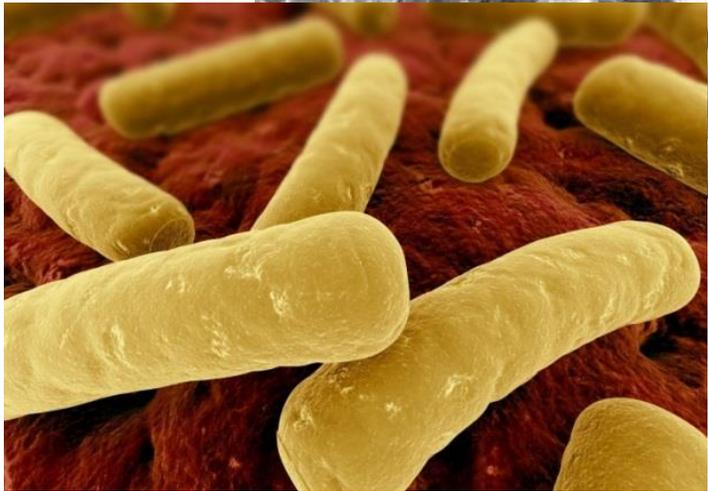
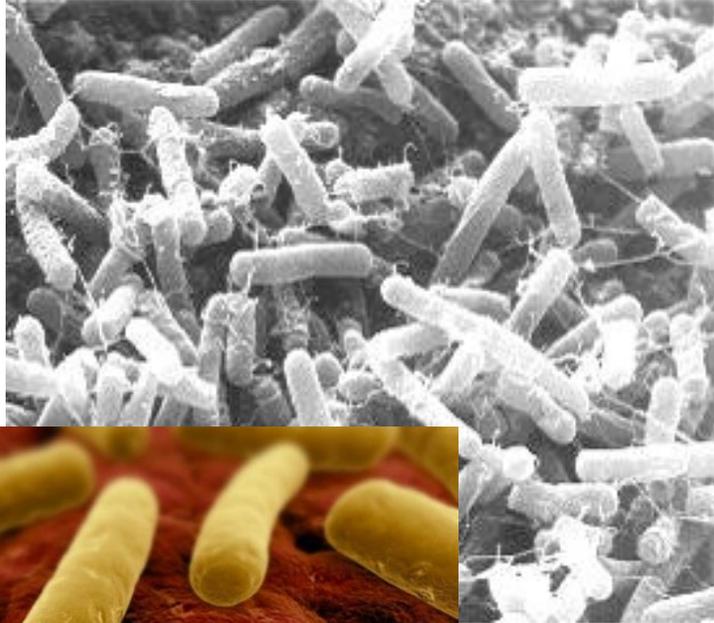
High heat

Easily converted into

No CO_2 or NO

- Highly functionalised compounds
- Industrial building block for polyhydroxyalkanoates production
- Drop-in biofuel: butyl-butyrate
n-butanol

Clostridium butyricum as vector for energy production

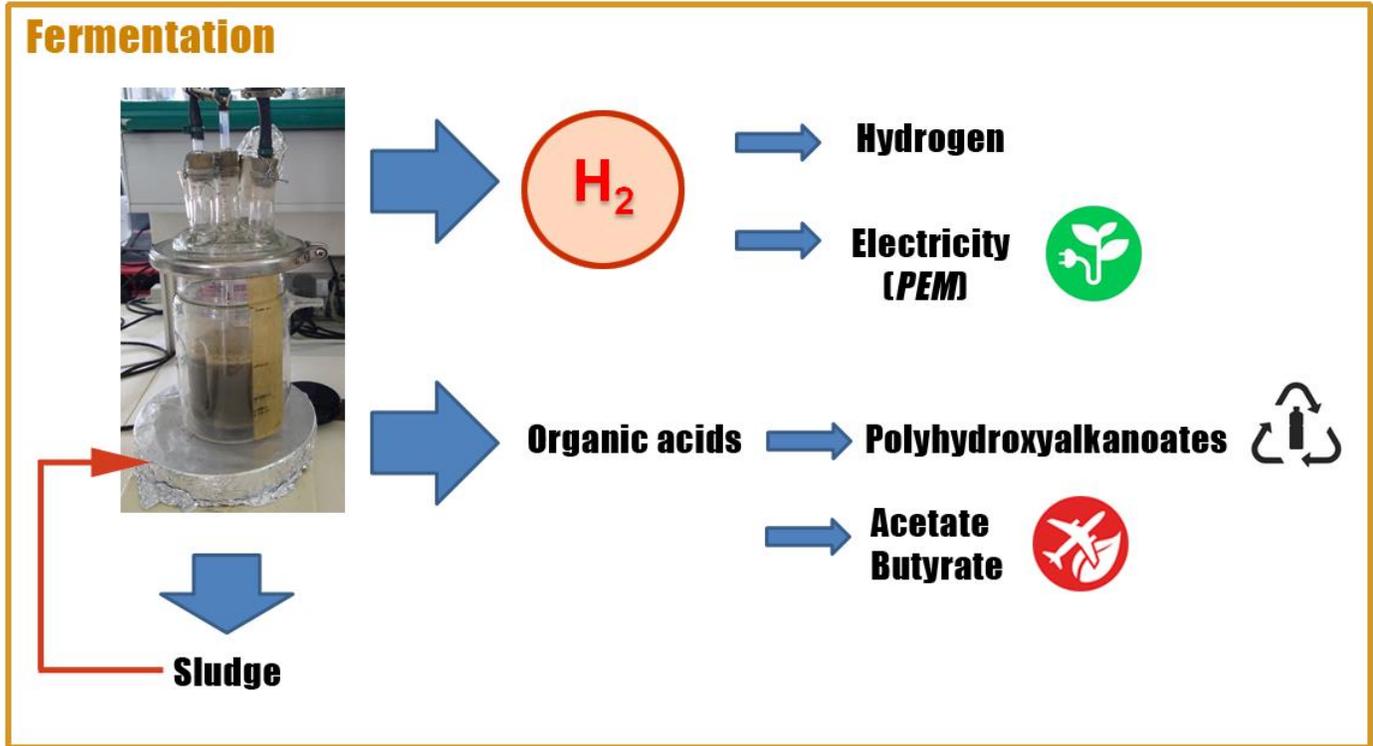
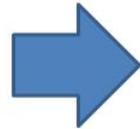


- Strict anaerobic bacteria.
- Extensive characterisation and subject to varied strain improvements
- Good H₂ producer.
- Capable of converting a wide range of substrates with high yields.
- Optimal pH 5.2-6.0

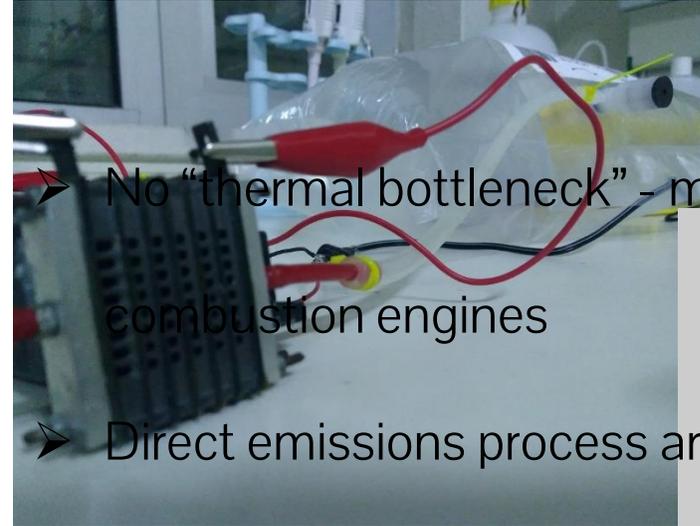
Proposed food waste biorefinery



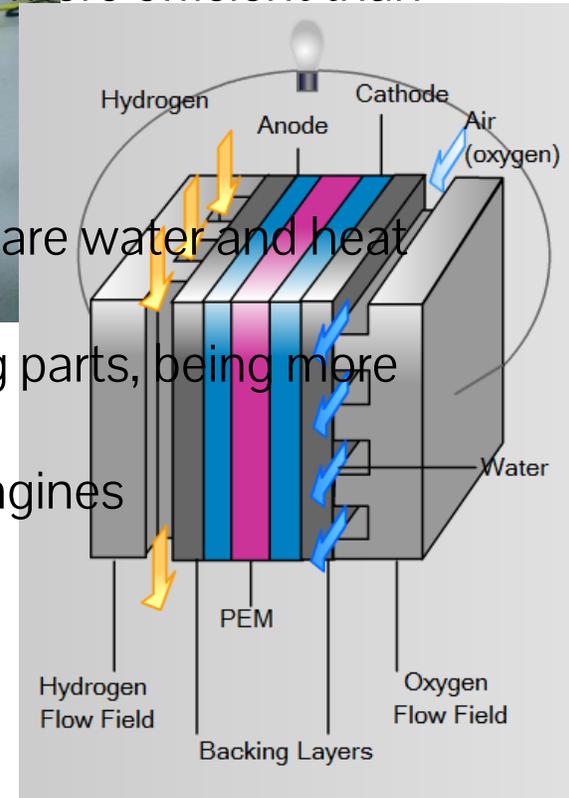
Food waste



Main product: H₂ to electricity

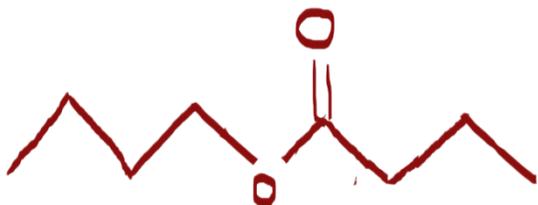


- No “thermal bottleneck” - more efficient than combustion engines
- Direct emissions process are water and heat
- Fuel cells have no moving parts, being more reliable than traditional engines



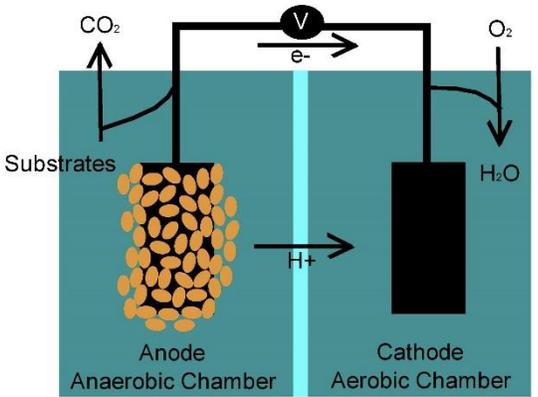
<http://www.hydrogenics.com/technology-resources/hydrogen-technology/fuel-cells/>

Byproduct: butyl-butyrate



- Esterified form of butyrate and butanol
- Thermochemical characteristics similar to fossil fuels
- Lower melting point
- Reduced hydrocarbons, sulfur and nitrogen oxides emissions
- Low aromatic content

Byproduct: electricity



- High conversion efficiency from substrate to energy
- Low temperature functioning
- Reduced hydrocarbons, sulfur and nitrogen oxides emissions
- No energy required for aeration of cathode
- Highly versatile system

Adapted from <https://www.labroots.com/trending/earth-and-the-environment/6010/methane-electricity-bacteria>

Substrate collection and processing



Seafood restaurant
kitchen waste



Removal of bones
and other foreign
materials

Mashing and
homogenisation



Fermentable FW biomass

Winter sampling (%_{d.w})

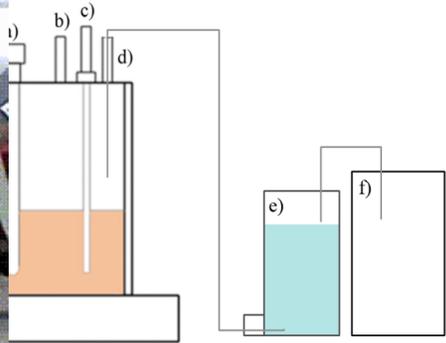
- 42% total sugars
- 24% crude protein
- 22% fat
- 2% ash

Summer sampling (%_{d.w})

- 62% total sugars
- 10% crude protein
- 26% fat
- 1% ash

Experimental set-up

- Small scale, no pH control
37 °C, 20 mL medium
- Bench scale, batch
37 °C, pH = 5.5
500 mL medium, 1.1

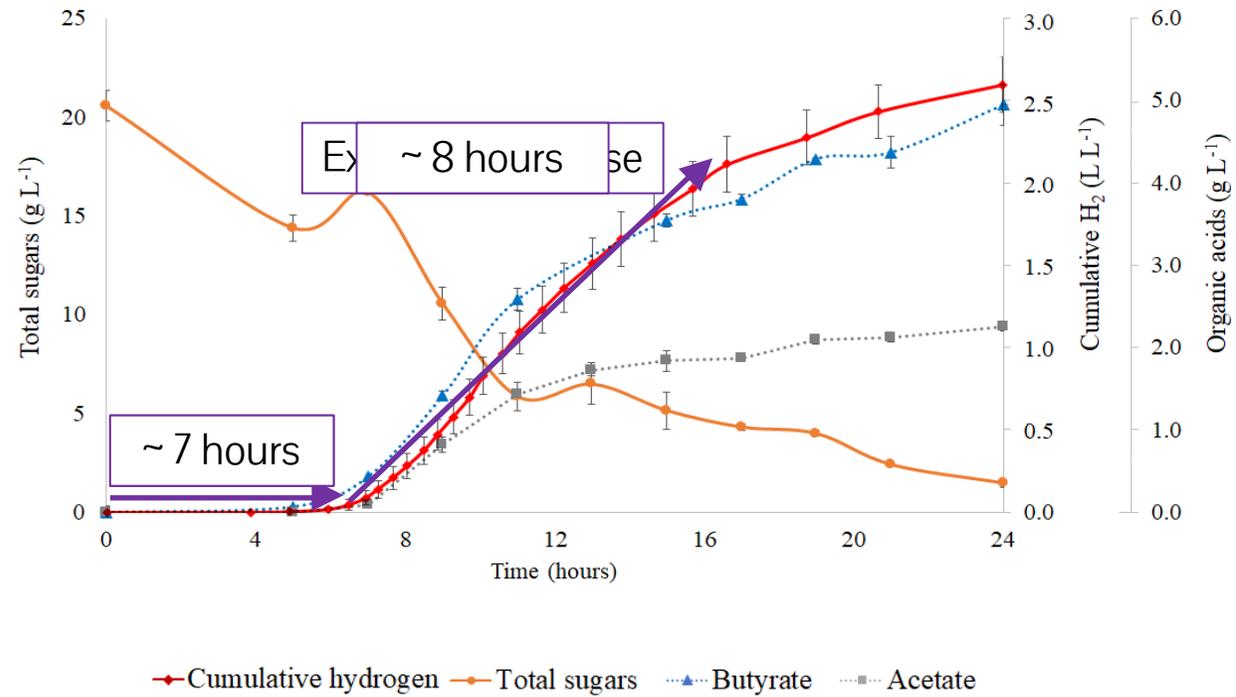


a) oxygen electrode
b) vacuum inlet
c) nitrogen inlet
d) Gas sampling exit
e) CO₂ scrubber
f) Sampling bag

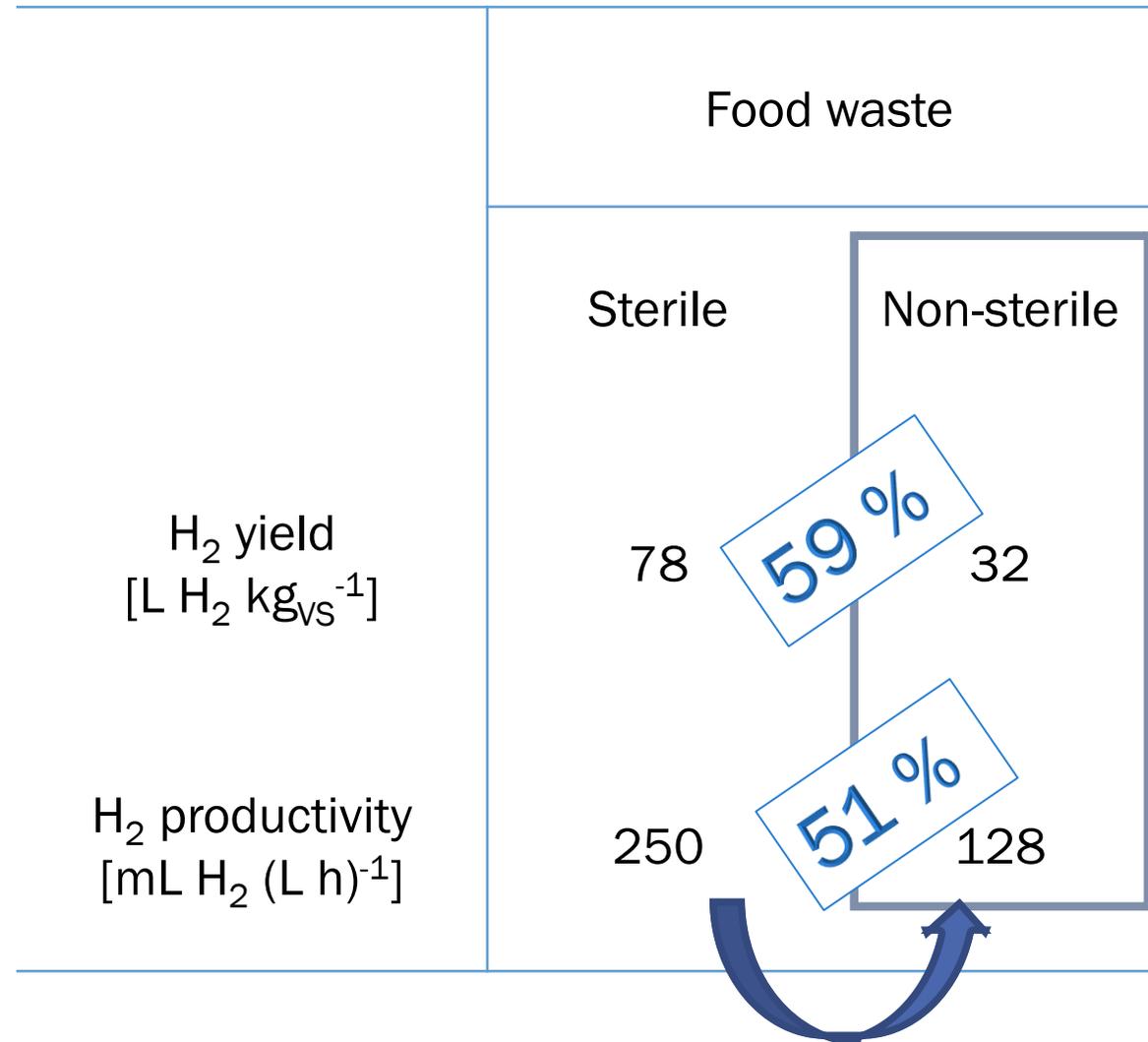
Quantification: H₂, C

ation, ash and H₂O

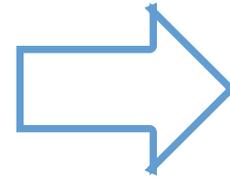
Food waste fermentation in bench-scale assay



Parameters	
Total H ₂ production [L L ⁻¹]	4.1
H ₂ yield [mL H ₂ g _{d.w.} ⁻¹]	78.4
H ₂ productivity [ml (L h) ⁻¹]	250
Final % H ₂ in the sample (% vol)	77
Sugar consumption (%)	86.5



Contamination control



- Contamination control
- Avoid further contamination - **Storage**

A - crude ground biomass

versus

B - Microwave pretreated biomass





In comparison with the **non-sterile condition**

Increase in H₂
yield
177 %

Increase in H₂
productivity
216 %

In comparison with the sterile condition

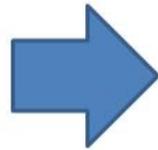
Increase in H₂
yield
14 %

Increase in H₂
productivity
63 %

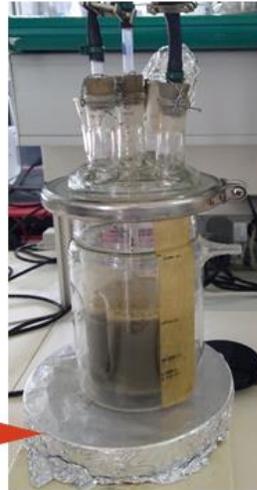
Proposed food waste biorefinery



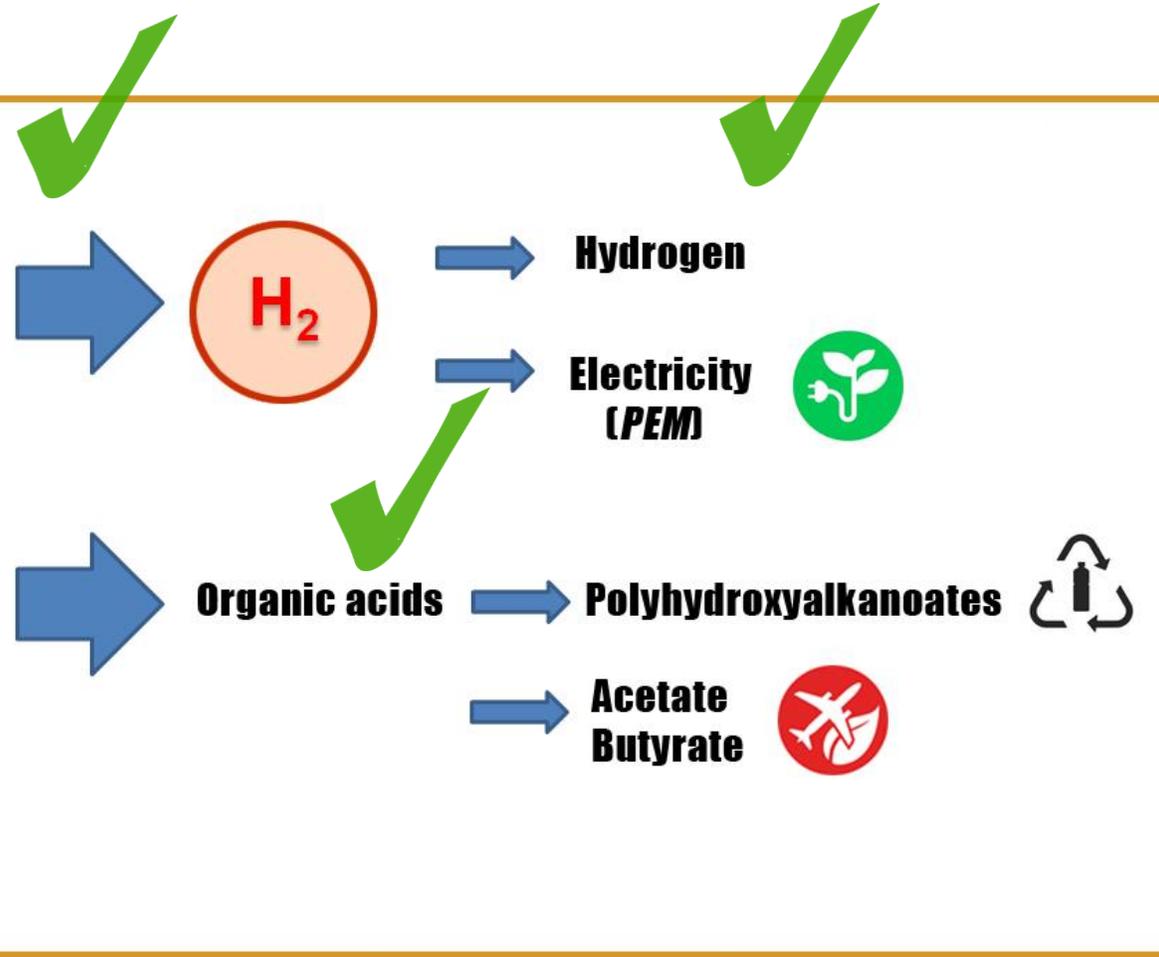
Food waste



Fermentation

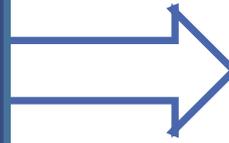


Sludge



Nitrogen source optimisation

Residual nitrogen in fermentate



- Limits polyhydroxyalkanoate (PHA) accumulation
- Nutrient waste

Nitrogen source reduction



Reduction by 66% of initial NH_4Cl concentration



Dark-fermentation sludge (%_{d.w})

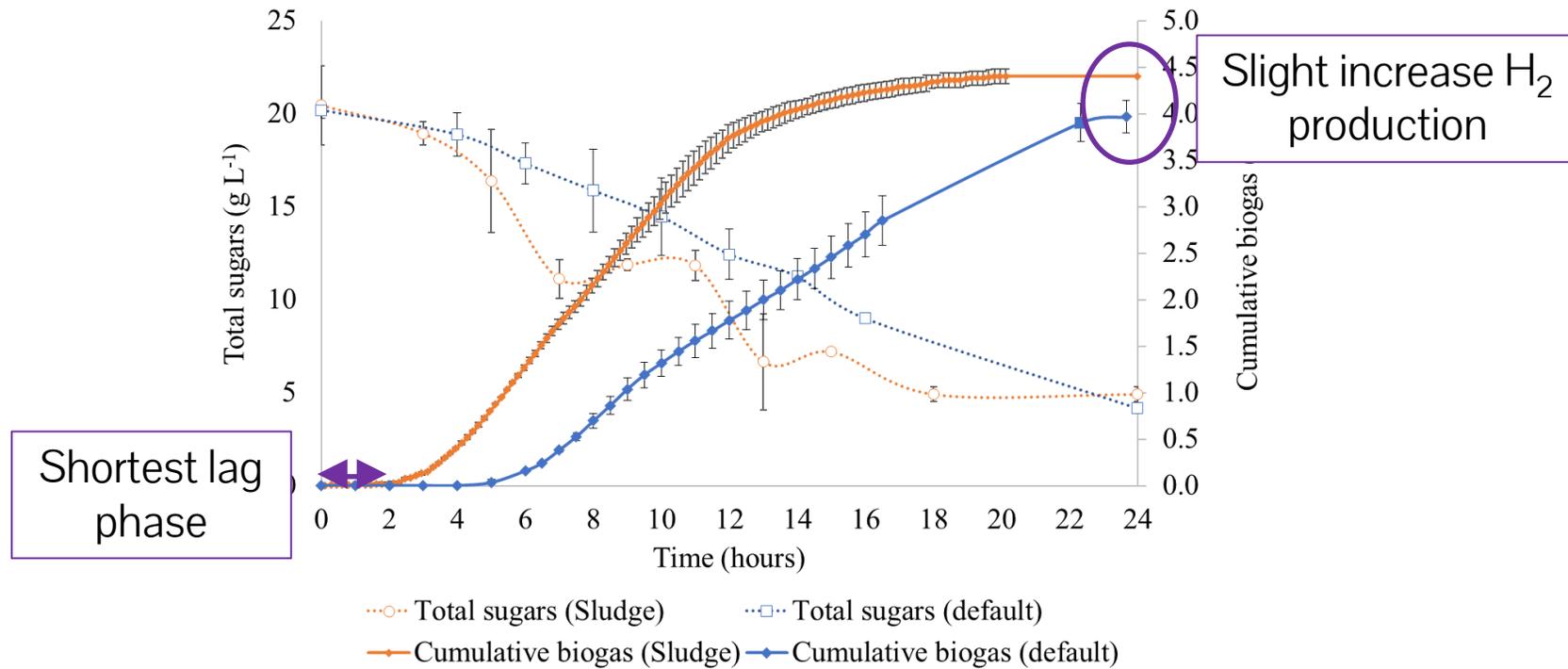
14% total sugars
58% crude protein

Nitrogen source replacement



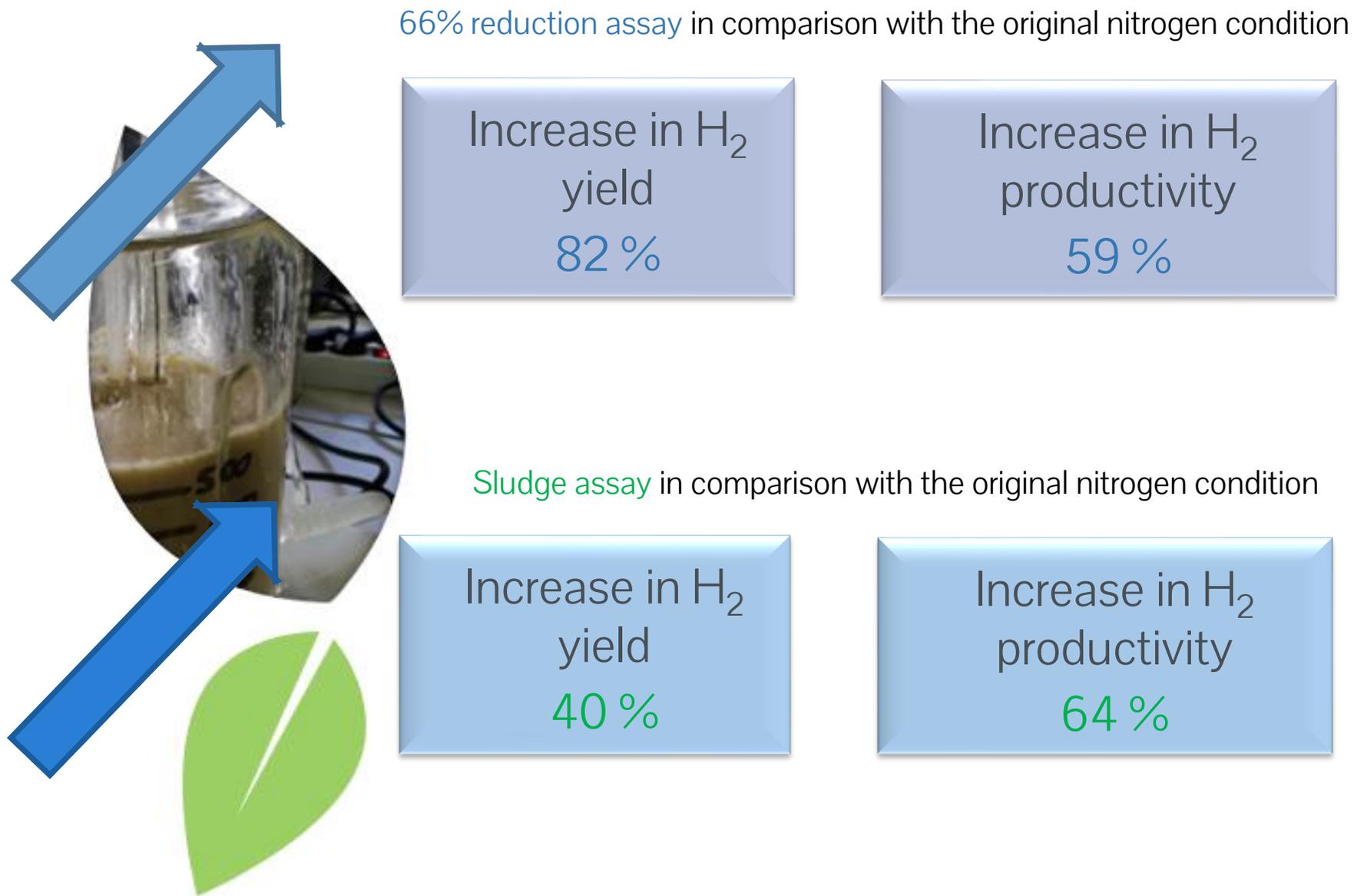
Replacement of NH_4Cl with DF-sludge

Food waste fermentation with nitrogen source replacement



Parameters	
Total H ₂ production [L L ⁻¹]	4.4
H ₂ yield [mL H ₂ g _{d.w.} ⁻¹]	111.9
H ₂ productivity [ml (L h) ⁻¹]	433.3
Final % H ₂ in the sample (% vol)	41
Sugar consumption (%)	75.9

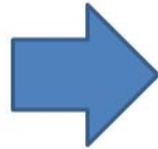




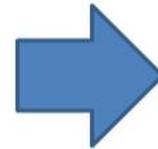
Proposed food waste biorefinery



Food waste



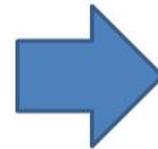
Fermentation



Hydrogen



**Electricity
(PEM)**



Organic acids



Polyhydroxyalkanoates



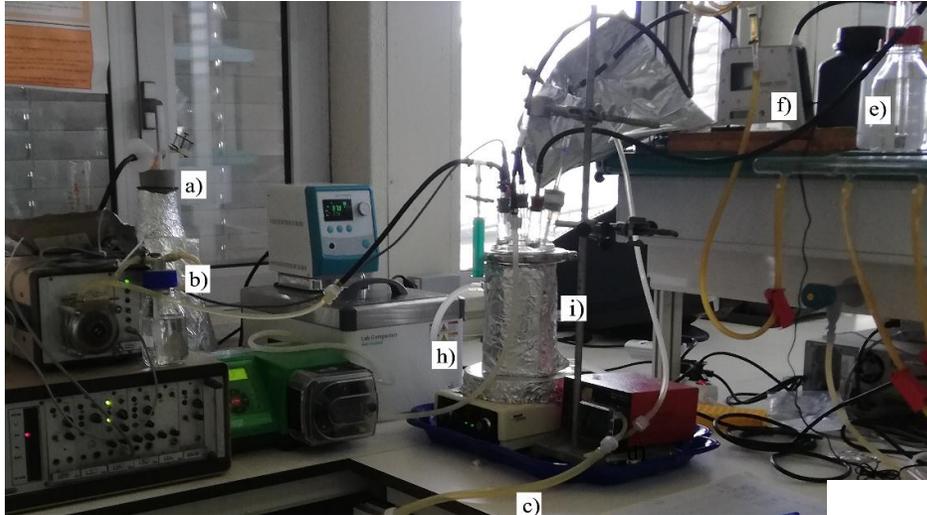
**Acetate
Butyrate**



Sludge



Experimental set-up



- a) Fermentation medium feed
- b) NaOH solution for pH control;
- c) Effluent
- d) Sampling port;
- e) CO₂ scrubber

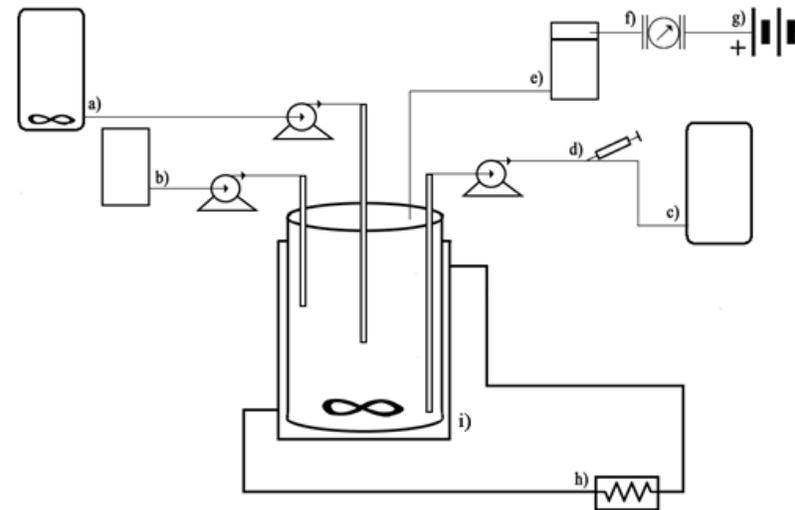
- f) Flowmeter;
- g) PEMFC;
- h) Water bath
- i) Biorreactor

Bench scale,
Optimum conditions for *C. butyricum*

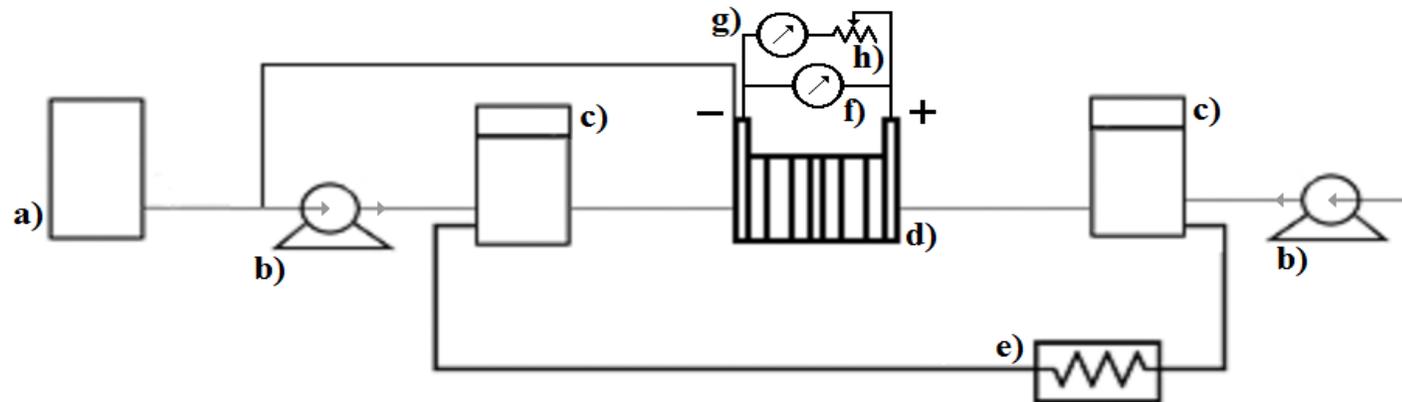
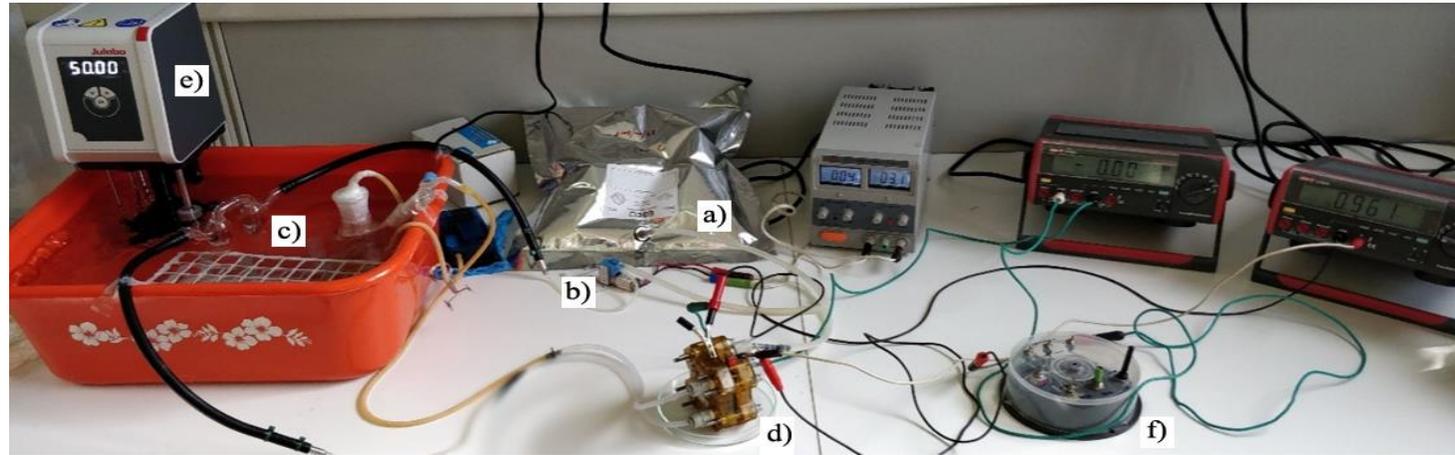
37 °C, pH = 5.5, 1.1 g sugars L⁻¹ h⁻¹

500 mL medium, 1.1 L headspace

FW Summer sampling



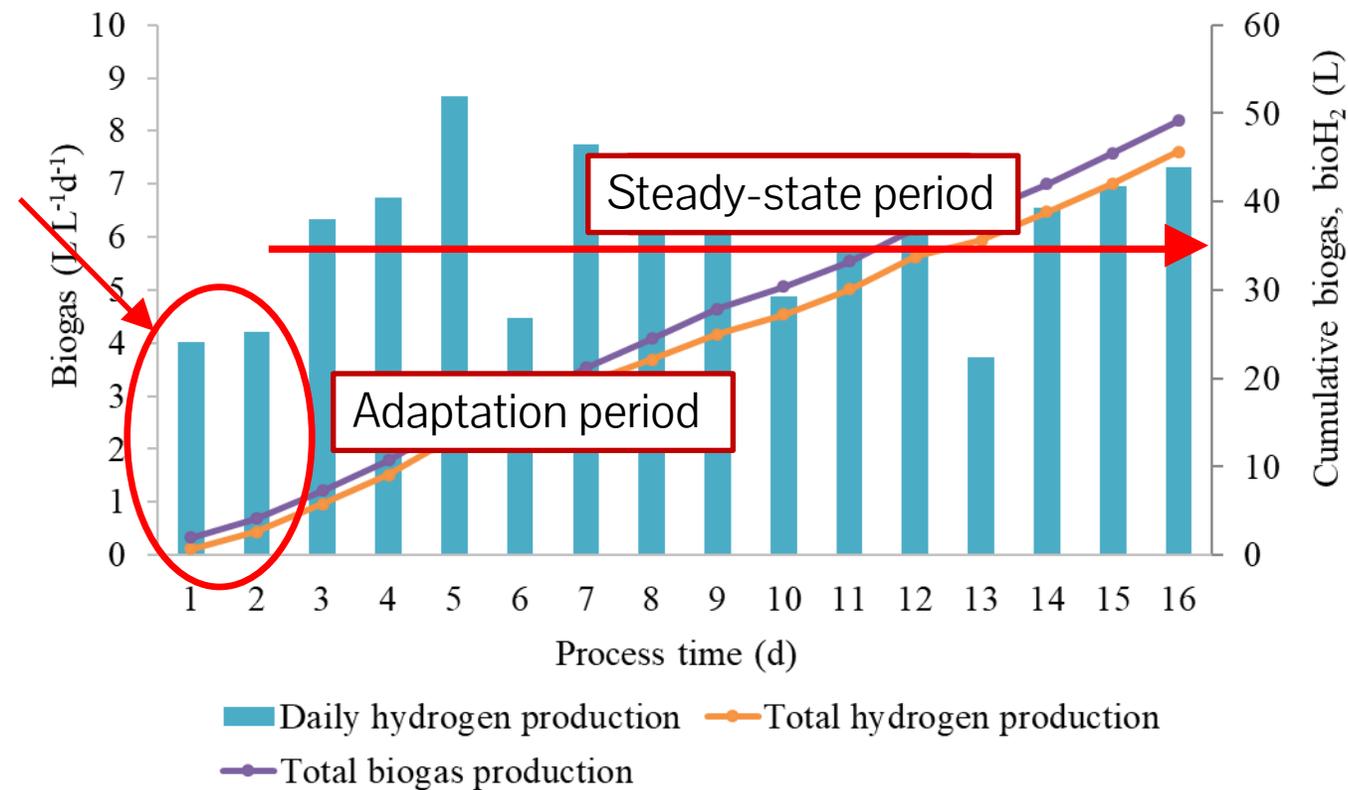
Quantification: H₂, CO₂, total sugars, organic acids, nitrogen concentration, ash and H₂O



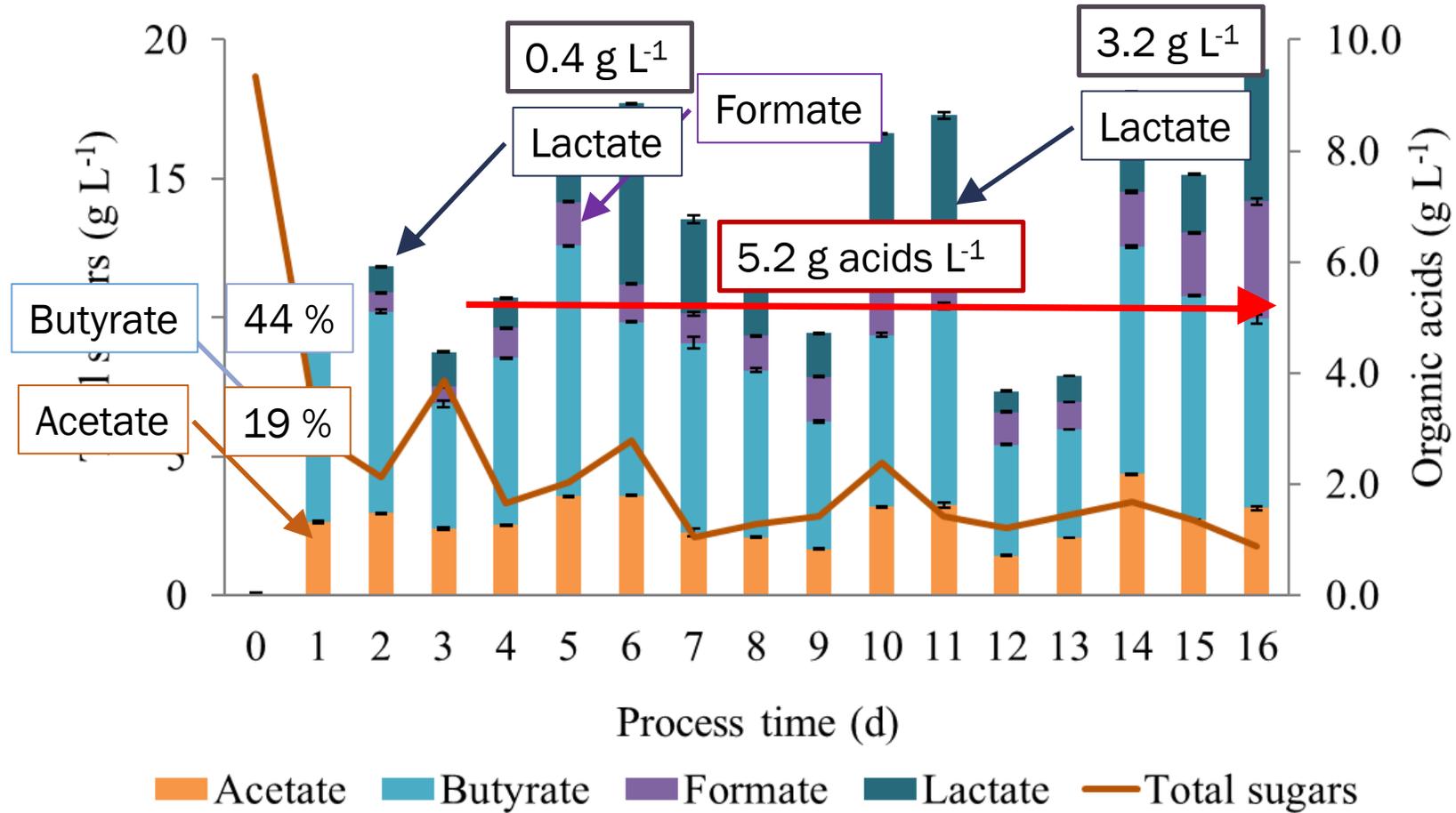
a) BioH₂ sample;
 b) Gas pump;
 c) Gas washing bottle;
 d) Fuel cell;

e) Water bath for temperature control;
 f) Voltmeter;
 g) Ammeter;
 h) Potentiometer

Food waste fermentation in CSTR mode

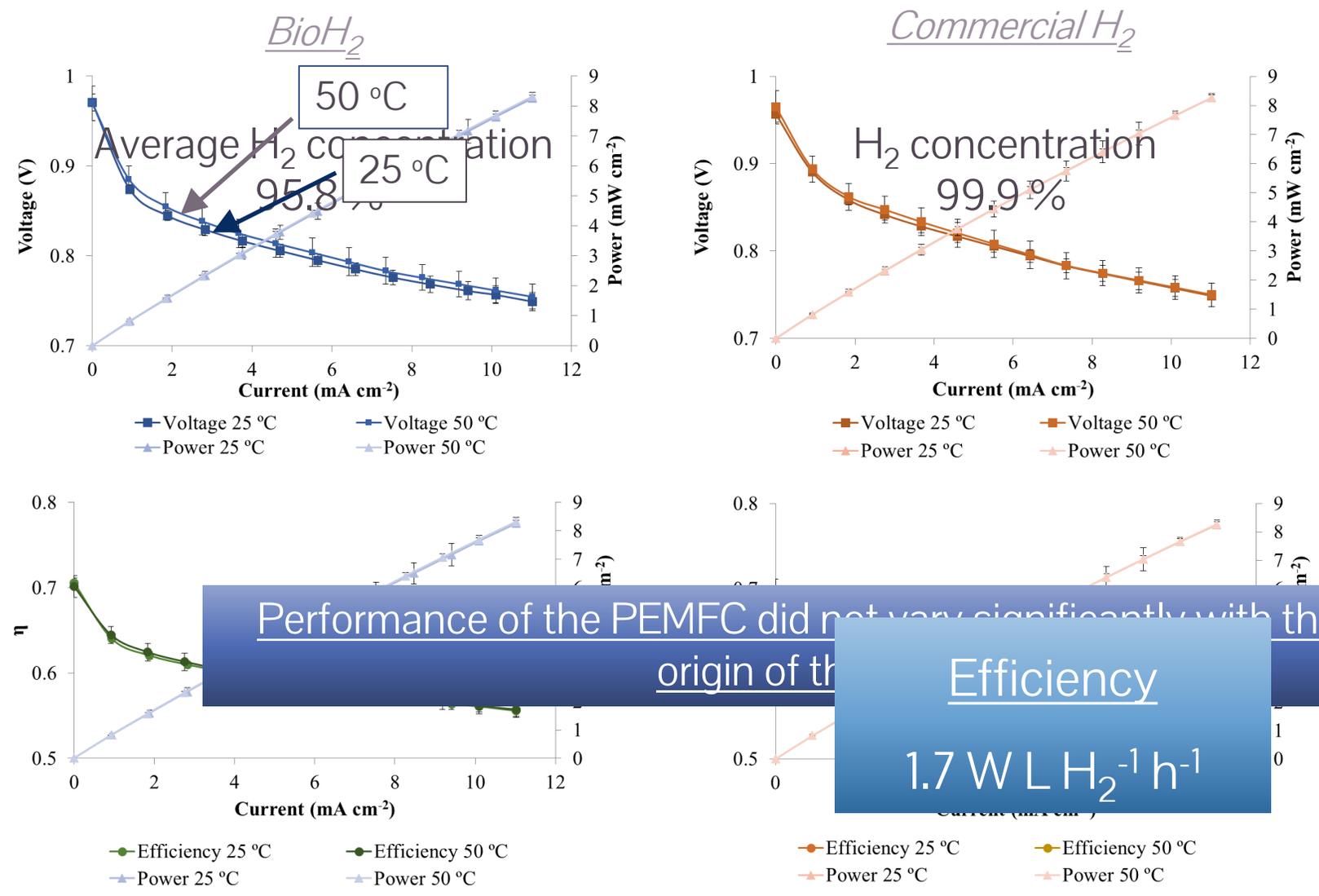


Parameters	
Total H ₂ production [$L L^{-1}$]	45.6
H ₂ yield [$L H_2 kg_{d.w.}^{-1}$]	74.9
H ₂ productivity [$L (L d)^{-1}$]	6.1
Average % H ₂ in biogas (% vol)	95.8
Sugar consumption (%)	94.1



Parameters	
Average organic acid concentration [g L ⁻¹]	5.2
Butyrate-to-acetate ratio [mol mol ⁻¹]	1.9

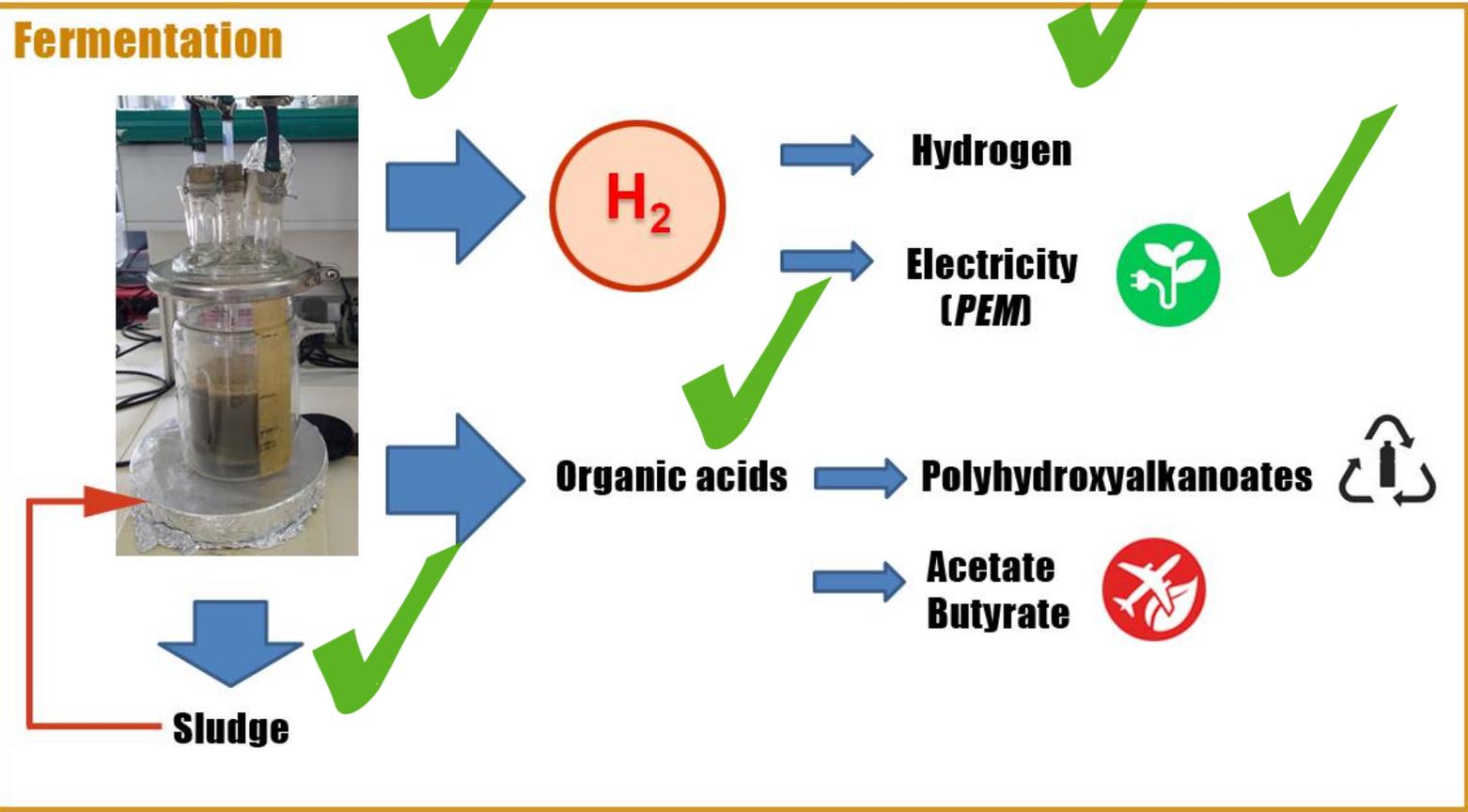
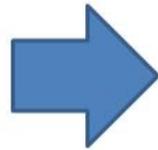
Electricity generation from bioH₂ with a PEMFC



Proposed food waste biorefinery

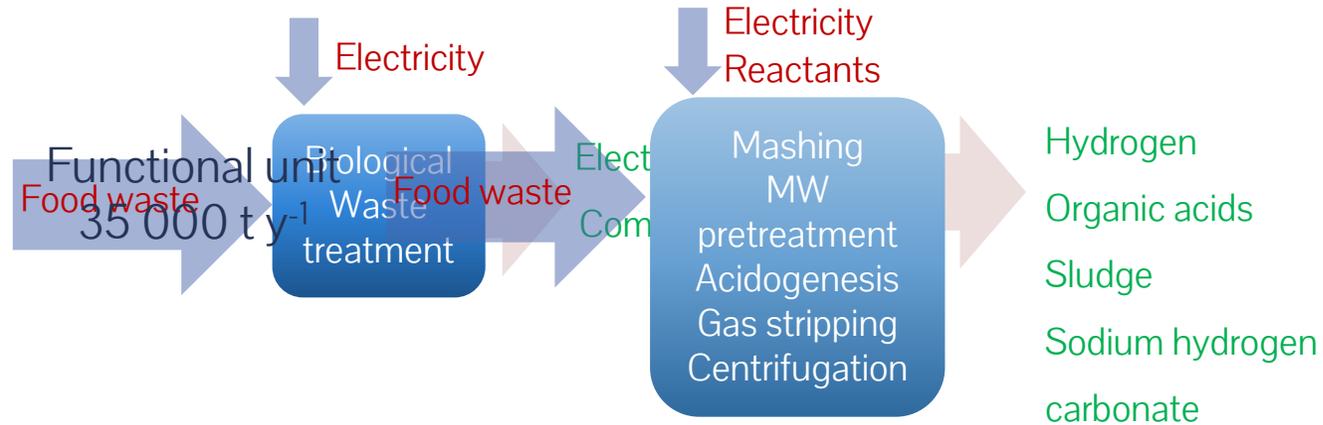


Food waste

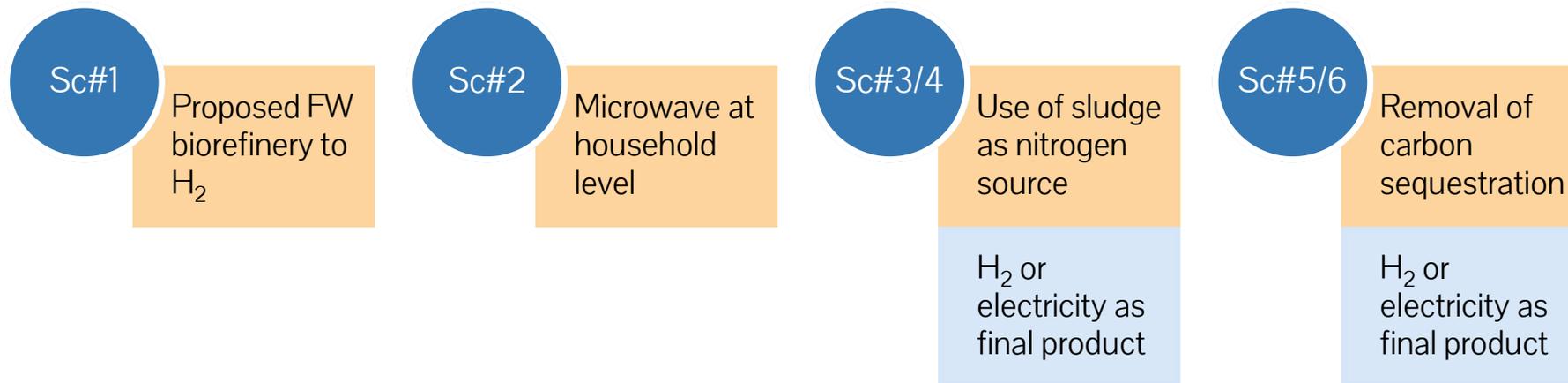


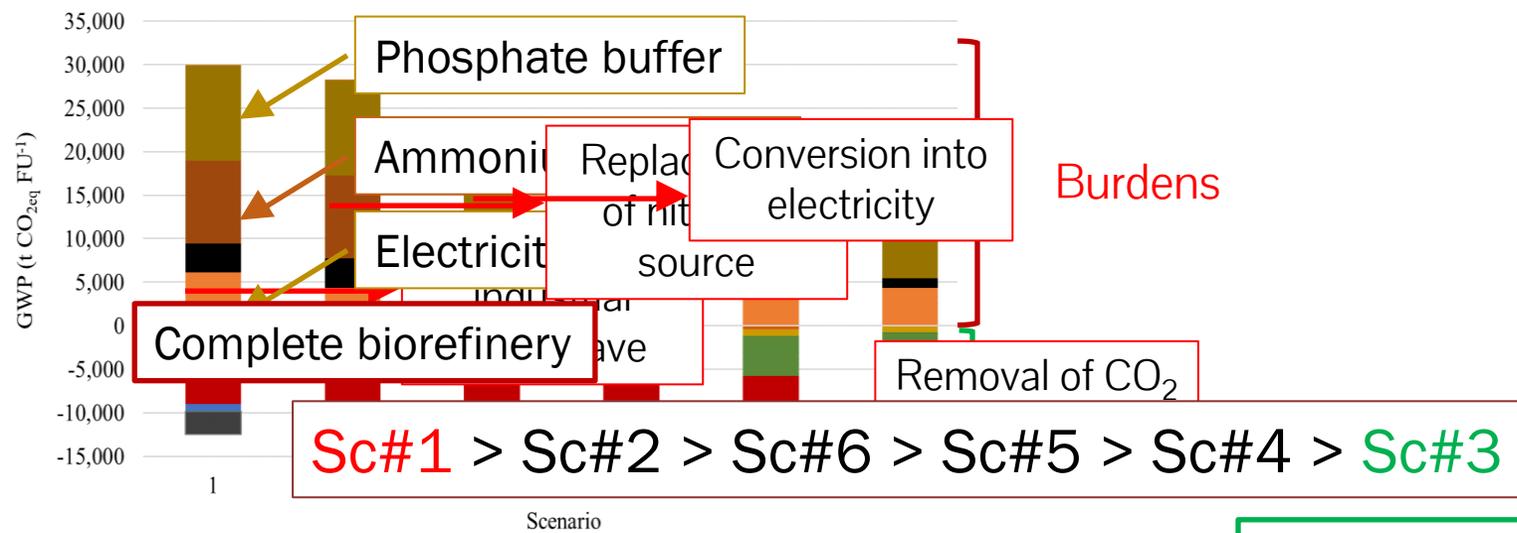
Process scale-up and scenario analysis

ValorSul reference Alternative system



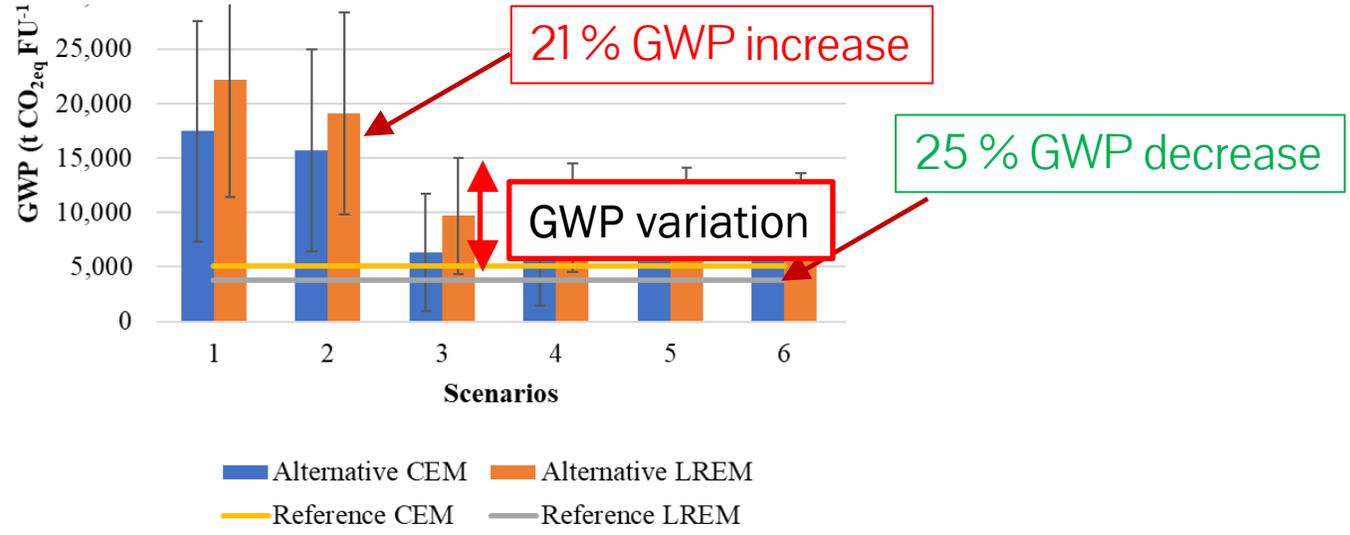
Global warming potential through consequential LCA





- Electricity
- Phosphate
- Biogenic
- Acetate
- Formate
- Sodium hydroxide
- Compost
- Sludge
- Butyrate
- Sodium hydrogen carbonate
- Ammonium chloride
- Iron sulphate
- Hydrogen
- Lactate
- Produced electricity

Use of sludge as nitrogen source



6.

Conclusions



Conclusions

- The restoration FW sampled was efficiently converted into H₂, attaining a maximum productivity of 250 mL (L h)⁻¹ and a conversion yield of 78.4 mL g_{d.w.}⁻¹.
- The removal of nutrient supplementation and sterilisation stage caused a decrease in all fermentation kinetic parameters, particularly the H₂ yield by 41 and 59% respectively.
- Microwave procedure was chosen as the most appropriate method for control of sample contamination prior to fermentation and possibly increase substrate biodegradability.
- Microwaved-FW fermentation was the most efficient of the four tested conditions:
 - Total H₂ production: 4.6 L L⁻¹
 - H₂ yield: 89.4 mL g_{d.w.}⁻¹
 - H₂ productivity: 406 mL (L h)⁻¹

- The two tested conditions for nitrogen optimisation impacted positively fermentation performance, increasing productivity by 49 and 64% for the reduction and replacement assays, respectively.
- H₂ yield obtained with DF-sludge was 111.9 mL H₂ g_{d.w.}⁻¹, which represents a 40% increase when compared to the default assay.
- The recycling of nutrients in non-sterile FW fermentations for H₂ production increases the overall process efficiency and reduces the need for additional nitrogen source.

- Acidogenic FW-fed CSTR was undertaken successfully under non-sterile conditions, with the predominance of the biocatalyst facilitated by the MW pretreatment, low HRT and optimum pH and temperature.
- During the 16 days of process time:
 - Average H₂ productivity: $6.1 \pm 1.3 \text{ L H}_2 \text{ L}^{-1} \text{ d}^{-1}$
 - H₂ % in biogas: $95.8 \pm 1.0 \%$
 - H₂ yield: $74.9 \pm 15.8 \text{ L H}_2 \text{ kg}^{-1}$
 - Acetate + butyrate concentration: $5.2 \pm 0.8 \text{ g L}^{-1}$
- Biogas was fed into PEMFC and its use compared with commercial H₂ at two temperatures. No significant difference was obtained at all tested conditions.
- Theoretical scale-up of the alternative system underlined that the replacement of ammonium chloride with acidogenic sludge for H₂ production was the best of the analysed scenarios.

Research papers and additional information

- ❑ Ortigueira J, Silva C, Moura P. Assessment of the adequacy of different Mediterranean waste biomass types for fermentative hydrogen production and the particular advantage of carob (*Ceratonia siliqua* L.) pulp. Int. J. Hydrogen Energy. 2018;43(16), 7773-7783.
- ❑ Ortigueira J, Martins L, Pacheco M, Silva C, Moura P. Improving the non-sterile food waste bioconversion to hydrogen by microwave pretreatment and bioaugmentation with *Clostridium butyricum*. Waste Manage. 2019;88:226-235.
- ❑ Ortigueira J, Moura P, Silva C. Dark fermentation sludge as nitrogen source for hydrogen production from food waste. In Wastes: Solutions, Treatments and Opportunities III: Selected Papers from the 5th International Conference Wastes 2019, September 4-6, 2019, Lisbon, Portugal (p. 301). CRC Press. 2019. ISBN: 9780429289798
- ❑ Ortigueira J, Pacheco M, Trancoso A, Farrancho P, Ferreira J, Silva C, Moura P. Food waste biorefineries: Stability of an acidogenic fermentation with carbon dioxide sequestration and electricity generation. J. Cleaner Prod. 2020.



INSTITUTO
DOM LUIZ



Ciências
ULisboa



TÉCNICO
LISBOA



Development and evaluation of an acidogenic biorefinery for food waste valorisation

- FCT grant: SFRH/BD/107780/2015
- This work is integrated in the project CONVERTE, supported by POSEUR (POSEUR-01-1001-FC-000001) under the PORTUGAL 2020 Partnership Agreement
- The author would like to acknowledge the financial support from FCT through project UIDB/50019/2020 – IDL and the support from the Biomass and Bioenergy Research Infrastructure (BBRI)- LISBOA-01-0145-FEDER-022059
- Dr. Jorge Correia, Dr. Paulo Lemos